

# **REINHOLD ENVIRONMENTAL Ltd.**



## **2011 APC Round Table & Expo Presentation**

July 11-12, 2011, in Cleveland, OH / Hosted by FirstEnergy

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# Cliffside 6 Integrated AQCS

## 2011 APC Round Table

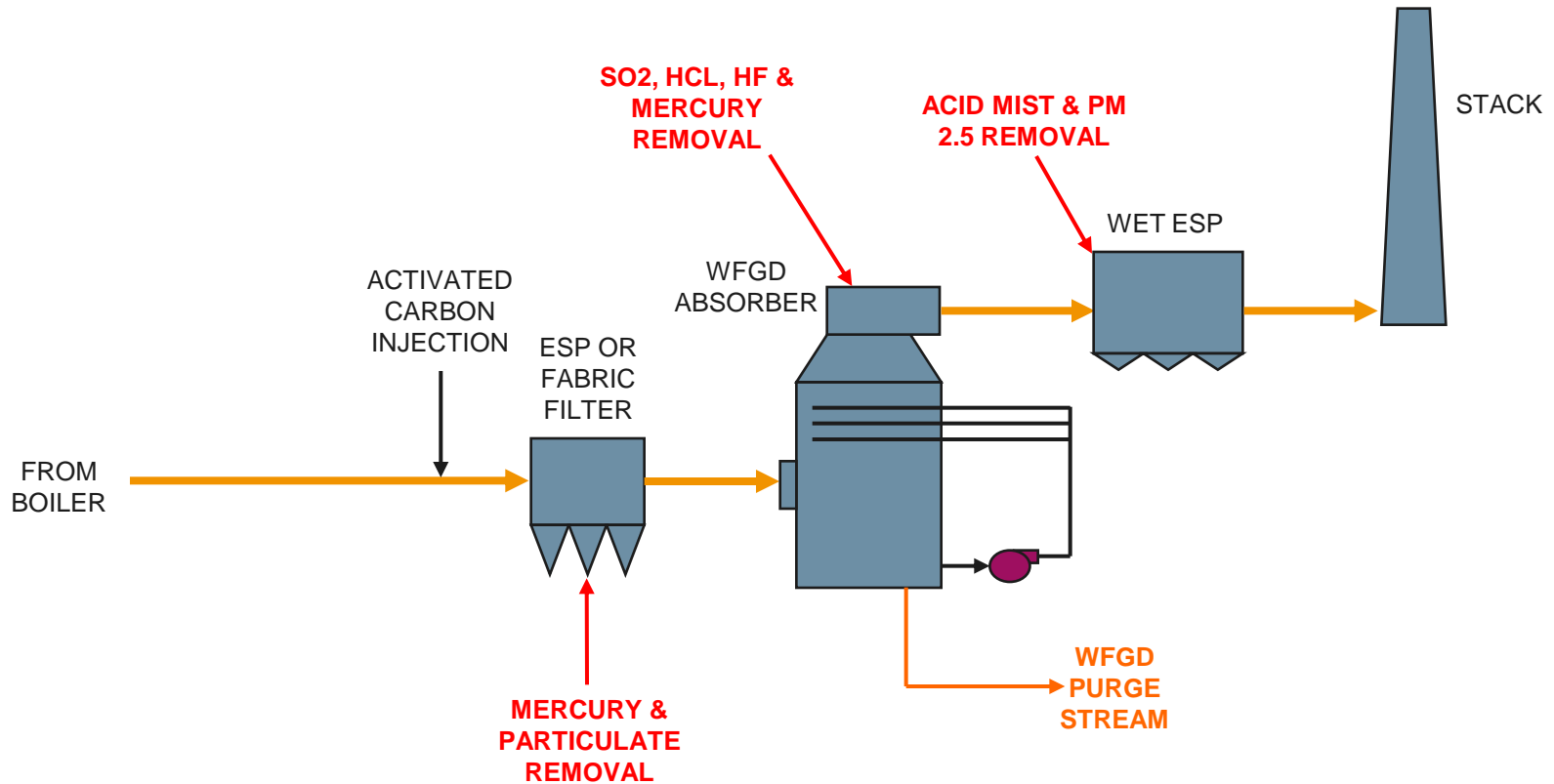
Phil Rader

Cleveland, OH – July 11, 2011

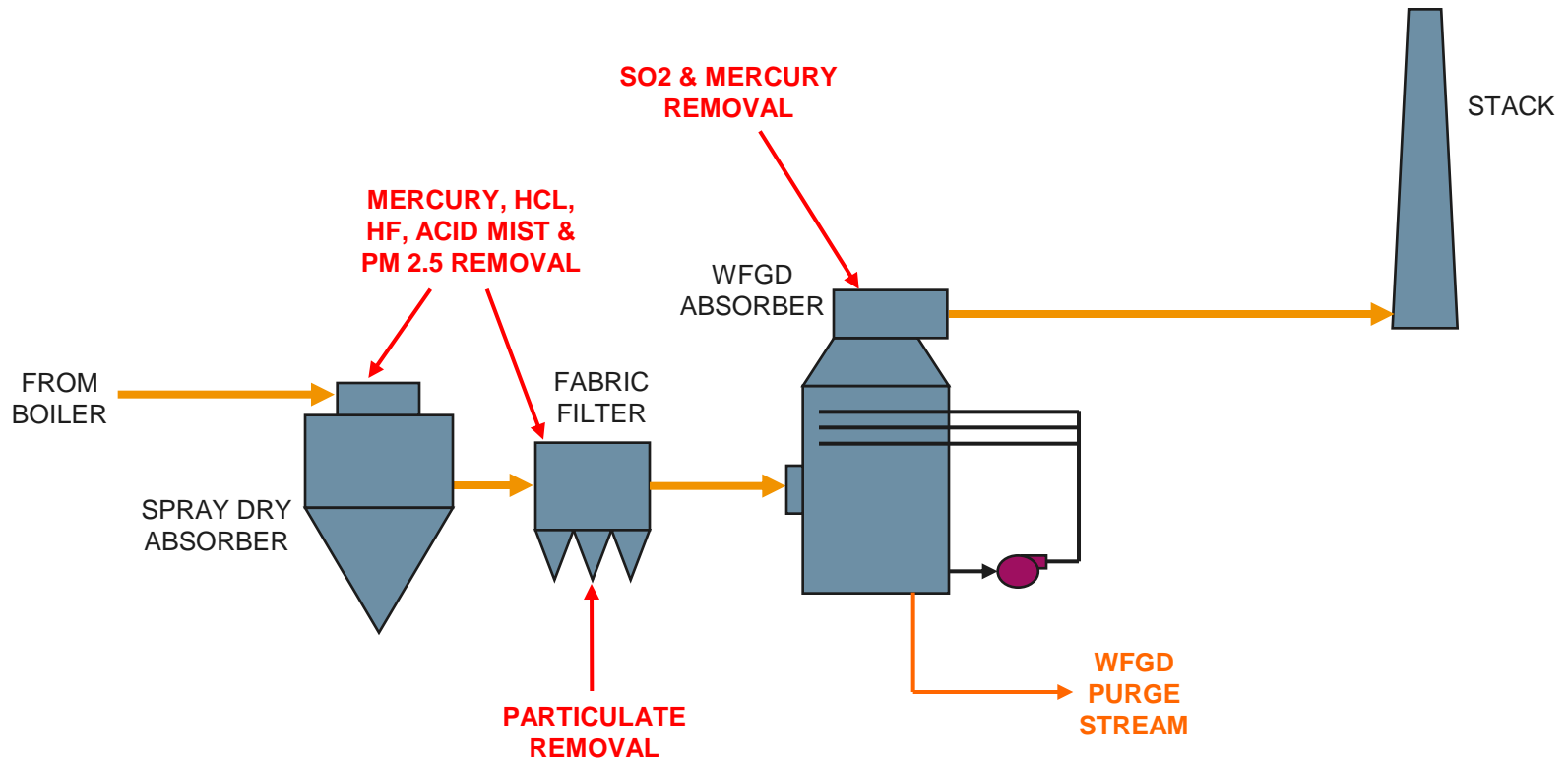
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# Conventional High Sulfur AQCS



# Integrated AQCS

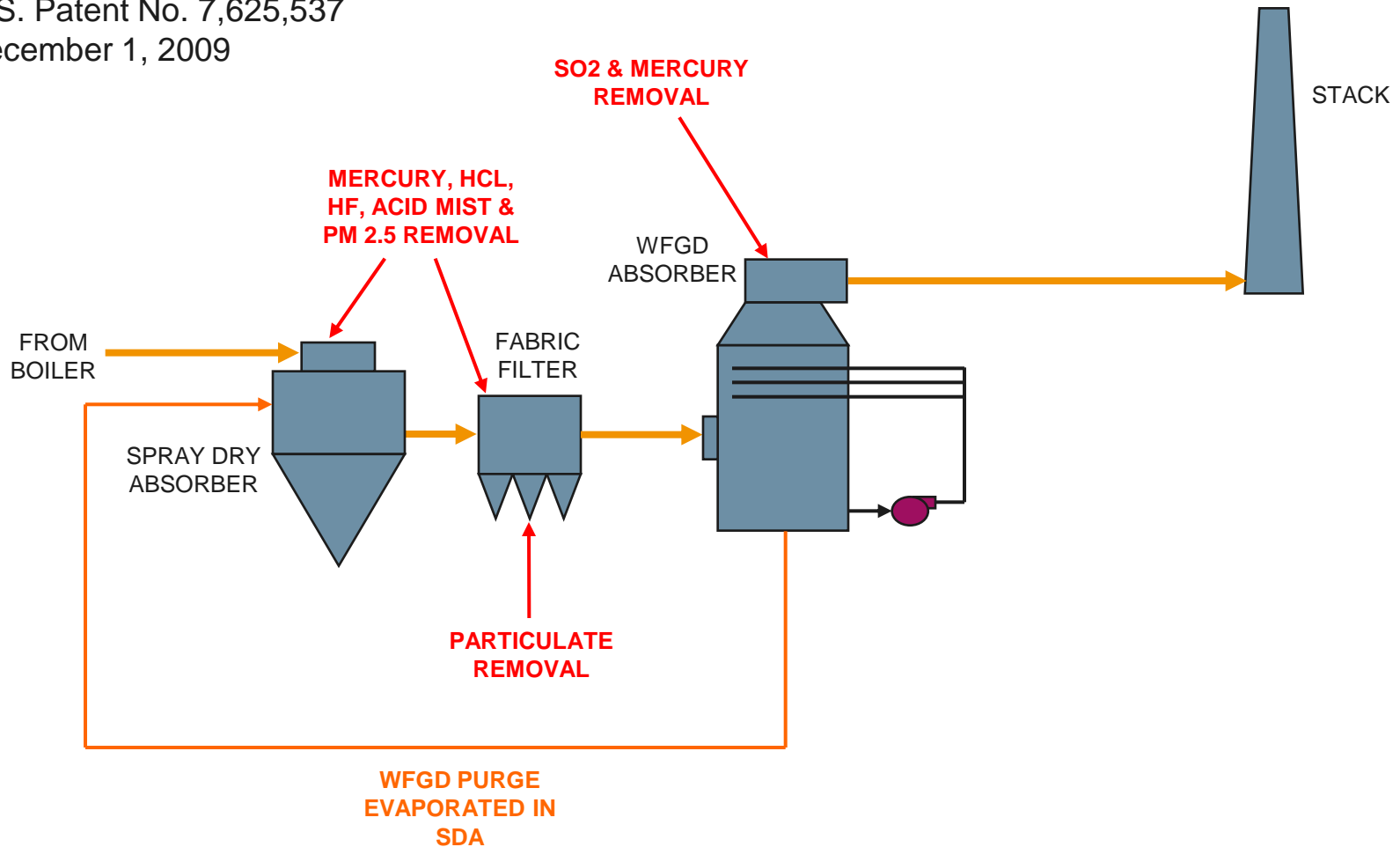


# Integrated AQCS

## INTEGRATED DRY AND WET FLUE GAS CLEANING PROCESS AND SYSTEM

U.S. Patent No. 7,625,537

December 1, 2009



- SDA/FF pilot plant (~1 MW) constructed at Cliffside Unit 5
- Testing carried out in Aug/Sept 2007
- Testing confirmed:
  - $\text{SO}_3$  emissions < 1 ppm
  - HCl vs.  $\text{SO}_2$  removal
  - Stoichiometric ratio
  - Byproduct composition



# SO<sub>3</sub> Control with DFGD

- Achieve total particulate emission and opacity limits without WESP
- Uses low cost lime reagent
- Compared to 800 MW plant with WESP:
  - Capital cost savings (~\$40-50 M)
  - O&M cost savings (\$1.0-1.5 M per year)
- Carbon steel SDA vs. alloy WESP
  - Lower material/erection cost
  - Less exposure to alloy price volatility
- WESP construction
  - Labor intensive
  - Significant alloy field welding



# No FGD Waste Water

- Eliminate wastewater treatment / disposal for AQCS
- Compared to 800 MW plant with WWTS:
  - Capital cost savings (~\$30-35 M)
  - O&M cost savings (\$1.0-1.5 M per year)
- Reduce land requirements
- Unit 5 waste water can also be accommodated by Unit 6 SDA under most circumstances

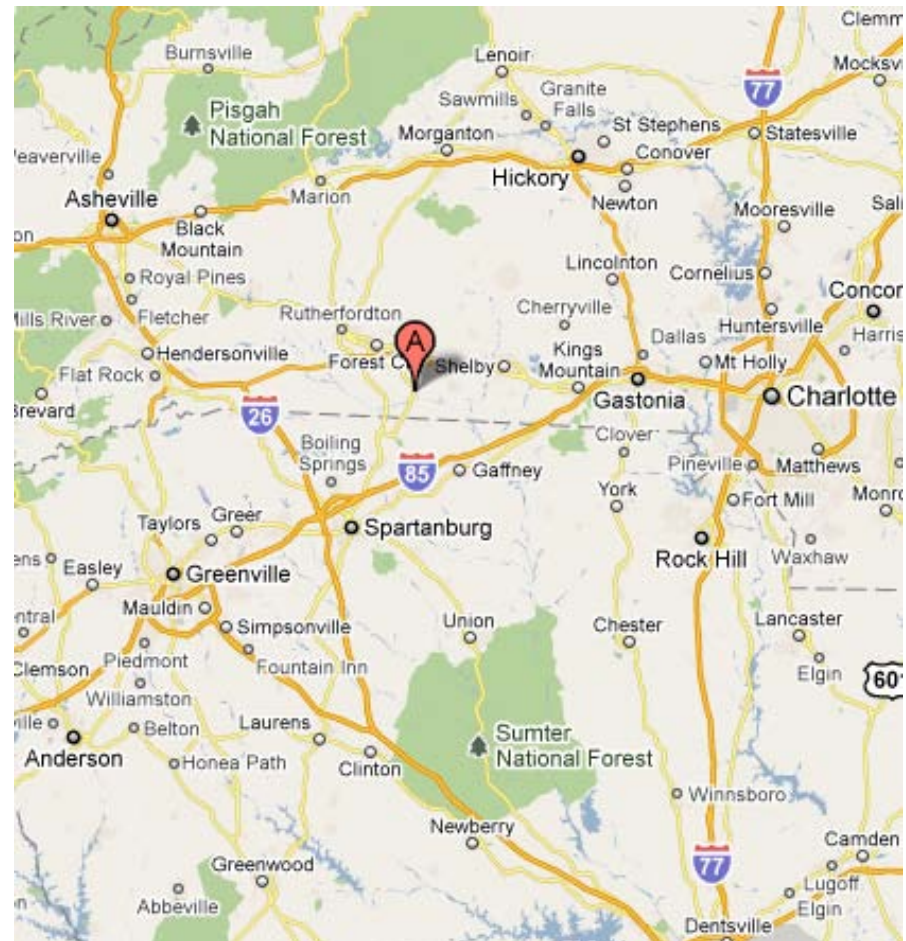


- Determined to be a minor source of HAPS
- Reduced WFGD material cost due to pre-collection of chlorides by DFGD
- Lower make-up water consumption
- Lower potential for Hg re-emission from WFGD
- Lower Hg levels in gypsum



# Cliffside Steam Station

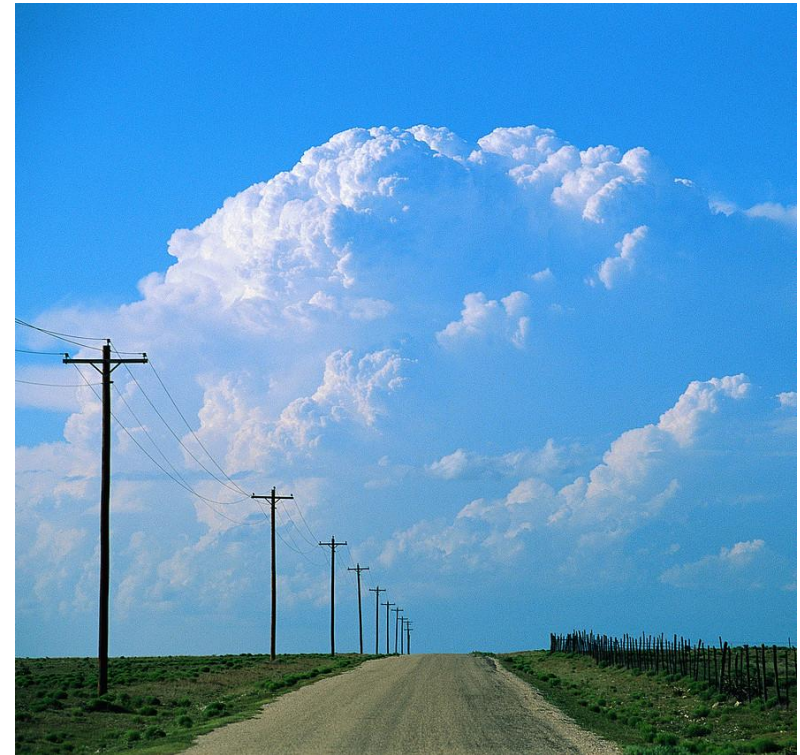
- Capacity: 760 MW
- Location: Cleveland and Rutherford Counties, NC
- Units 1-4 on-line in 1940s
- Unit 5 (560 MW) on-line in 1972
  - ESP initially
  - SCR in 2002
  - WFGD in 2010
- Unit 6 (825 MW) on-line in 2012
  - SCR
  - Integrated AQCS (SDA/FF/WFGD)



# Cliffside Plant Overview



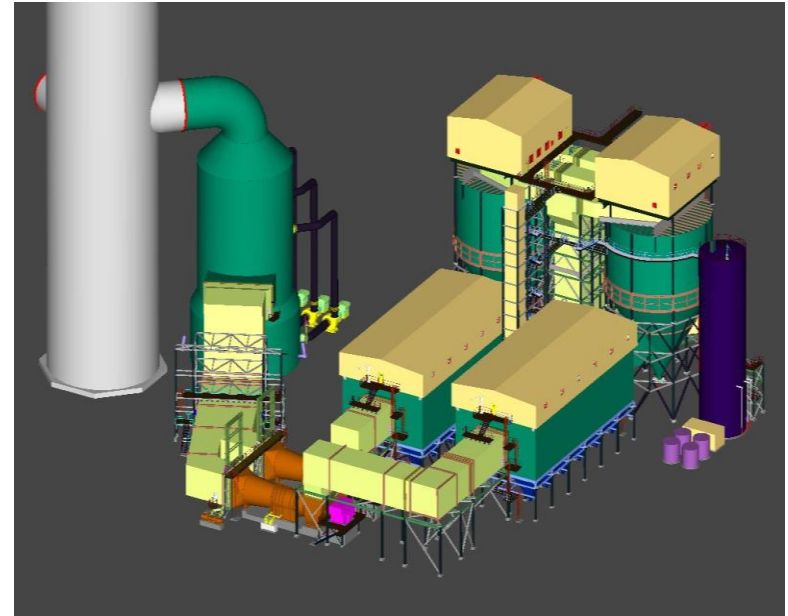
- Permit issued by DENR on January 29, 2008
- Compared to the existing plant, the modernized plant will emit 80% less SO<sub>2</sub>, 50% less NO<sub>x</sub>, and 50% less Hg while generating more than twice the electricity
- Permitted as a “minor source” of HAPS
- Awarded US Department of Energy clean coal tax credit of \$125 million
- First US coal plant to include CO<sub>2</sub> mitigation plan – requires Duke to retire an additional 800 MW by 2018



# Duke Energy Cliffside 6 Integrated AQCS



<b>Project Scope</b>	Spray dryer, fabric filter, spray tower, lime/limestone preparation and feed systems, by-product dewatering system, ductwork, fans, erection and commissioning advisors
<b>Location</b>	Cliffside, NC
<b>Capacity</b>	825 MW
<b>Start-Up</b>	May 2012
<b>Fuel</b>	Eastern Bituminous
<b>Spray Dryers</b>	Two 68 ft dia SDAs; three 200 hp atomizers per SDA
<b>Fabric Filter</b>	Two 12-compartment casings; 8-meter PPS/P84 blend bags
<b>Spray Tower</b>	One 61 ft dia tower; 5 spray levels
<b>Reagent</b>	Lime, limestone
<b>By-product</b>	Commercial gypsum



Duke Energy  
Cliffside Unit 6  
Cliffside, NC

# Cliffside 6 Construction



# Cliffside 6 Construction



# Cliffside 6 Construction



# Cliffside 6 Construction





# Cliffside 6 Construction



Cliffside 6 Integrated AQCS - July 2011

# Lifecycle Cost Analysis



<b>Technology</b>		<b>Integrated FGD</b>	<b>FF/WFGD/WESP</b>
Total Plant Capital Cost	\$	240,000,000	310,000,000
Normalized Capital Cost	\$/kW	300	388
Plant Capacity (per unit)	MWe	800	800
No. Units		1	1
Plant Capacity Factor	%	85	85
Equivalent Annual Operating Hours	hr	7,446	7,446
Escalation Rate	%	4.0	4.0
NPV Discount Rate	%	10.0	10.0
SO2 Production Rate	lb/hr	26,386	26,386
ID Fan Flue Gas Flow	acfm	2,562,000	2,692,035

# Lifecycle Cost Analysis

<b>Technology</b>		<b>Integrated FGD</b>	<b>FF/WFGD/WESP</b>
Total FGD Power	kW-hr/hr	14,225	15,587
Power Cost	\$/kW-hr	0.030	0.030
Pressure Drop	in. w.g.	36.5	34.5
Booster Fan Power Consump	kW-hr/hr	13,714	13,620
Total Power	kW-hr/hr	27,939	29,207
Limestone Consumption	ton/hr	32.0	32.6
Limestone Cost	\$/ton	20.00	20.00
Lime Consumption	ton/hr	1.3	0.0
Lime Cost	\$/ton	110.00	110.00
Alkali Used		NA	MgO
Alkali Consumption	ton/hr	0.0	0.2
Alkali Cost	\$/ton	0.00	400.00
Gypsum Production	ton/hr	74.0	75.5
Repair/Maintenance	% of TPC	1.5	1.5

# Lifecycle Cost Analysis



<b>Technology</b>	<b>Units</b>	<b>Integrated FGD</b>	<b>FF/WFGD/WESP</b>
Auxiliary Power	\$/yr	6,241,001	6,524,350
Limestone	\$/yr	4,765,440	4,860,749
Lime	\$/yr	1,064,778	0
Alkali Injection	\$/yr	0	648,789
WWTS Reagents	\$/yr	0	1,300,000
Gypsum	\$/yr	(2,755,020)	(2,810,120)
Repair/Maintenance	\$/yr	3,600,000	4,650,000
Total	\$/yr	12,916,199	15,173,767
	\$/MW-hr	2.17	2.55
<b>Total Plant Capital Cost</b>	<b>\$</b>	<b>240,000,000</b>	<b>310,000,000</b>
<b>NPV (20 years) - Total Annual C</b>	<b>\$</b>	<b>145,160,000</b>	<b>170,530,000</b>
<b>Total Lifecycle Cost</b>	<b>\$</b>	<b>385,160,000</b>	<b>480,530,000</b>

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